

# Battery Modeling: Trade-offs between Accuracy and Complexity

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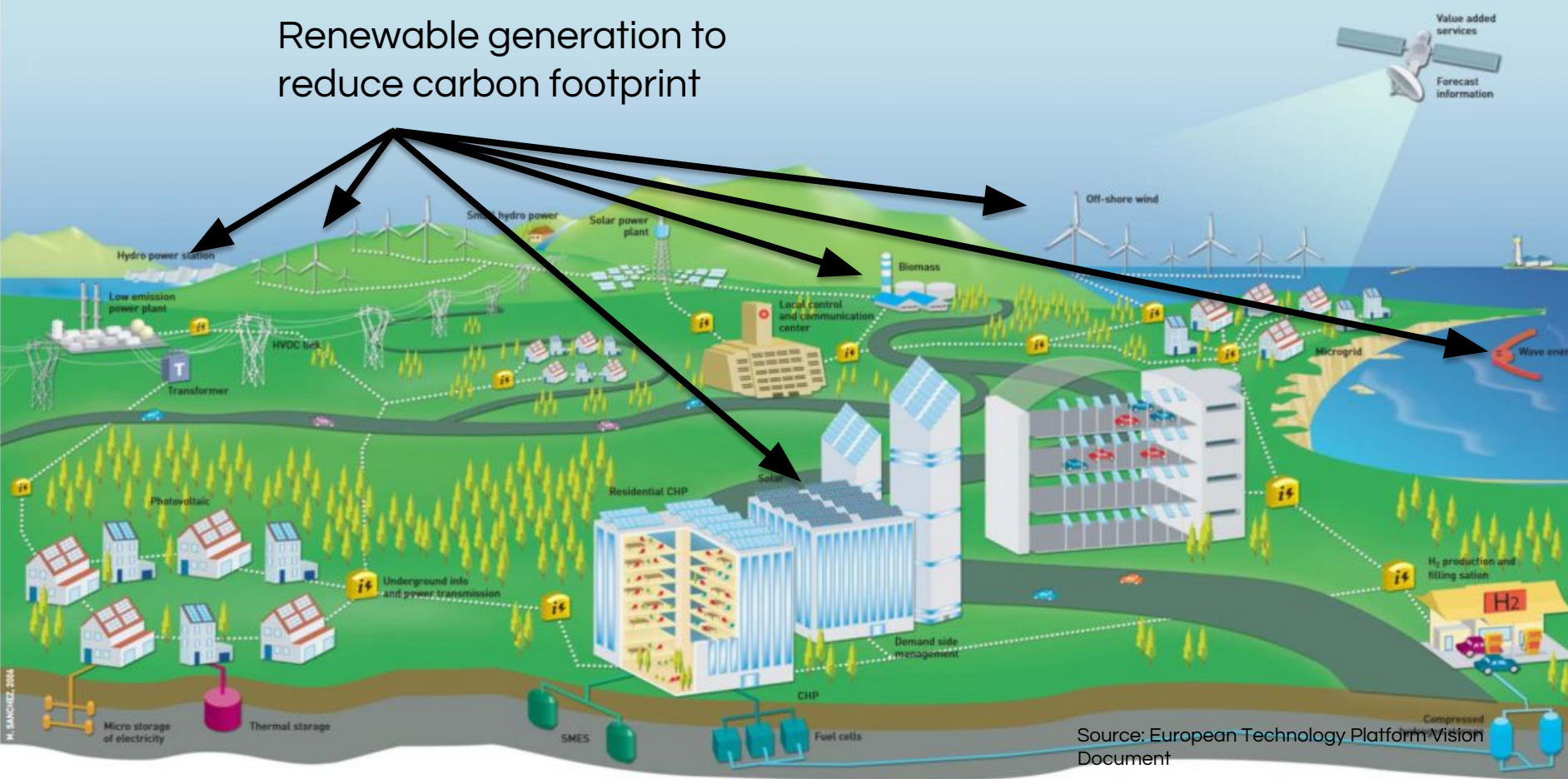
Cisco Research Chair in 5G Systems

# Smart Grid



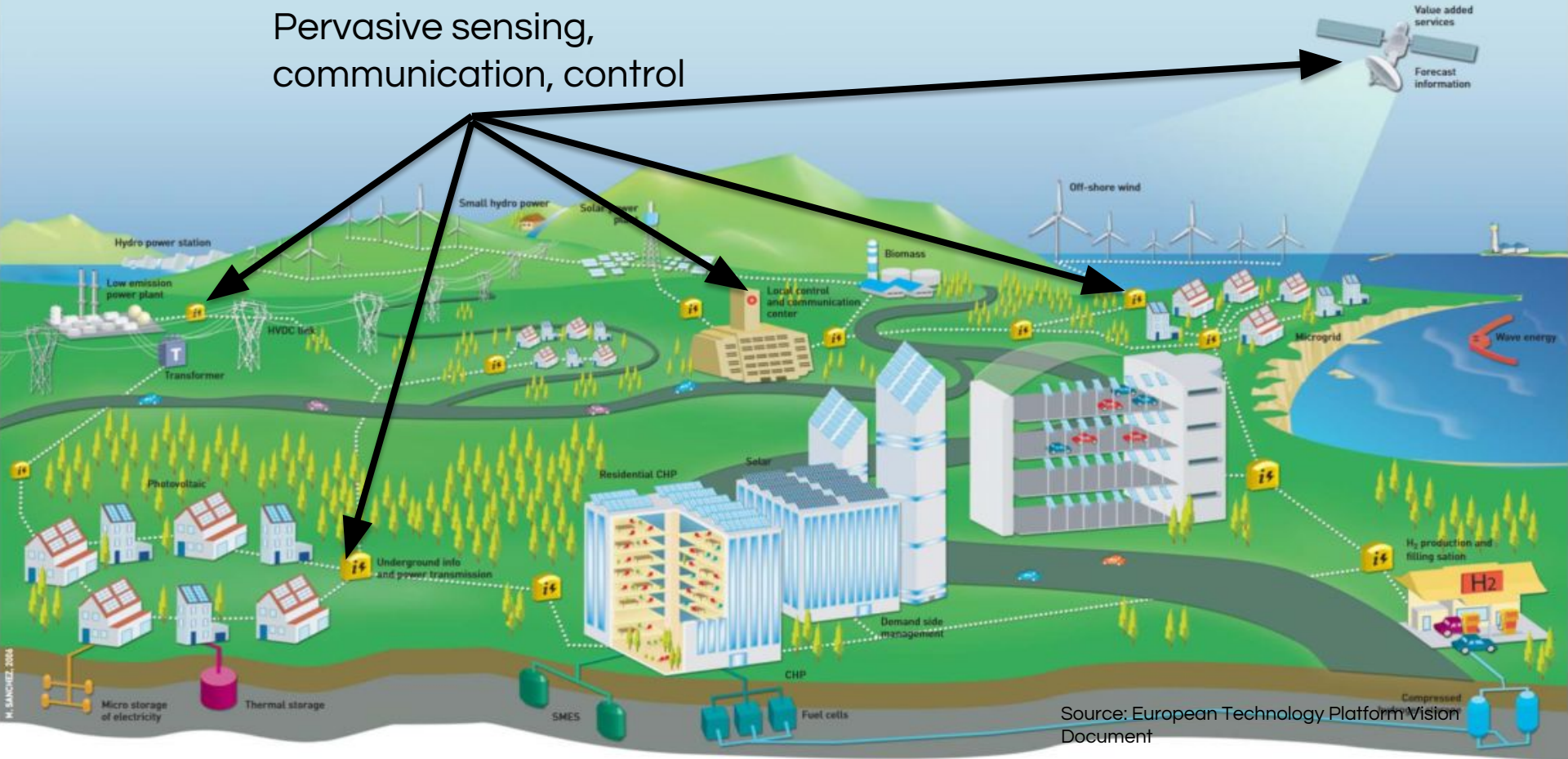
M. LAMOREZ, 2008

# Renewable generation to reduce carbon footprint



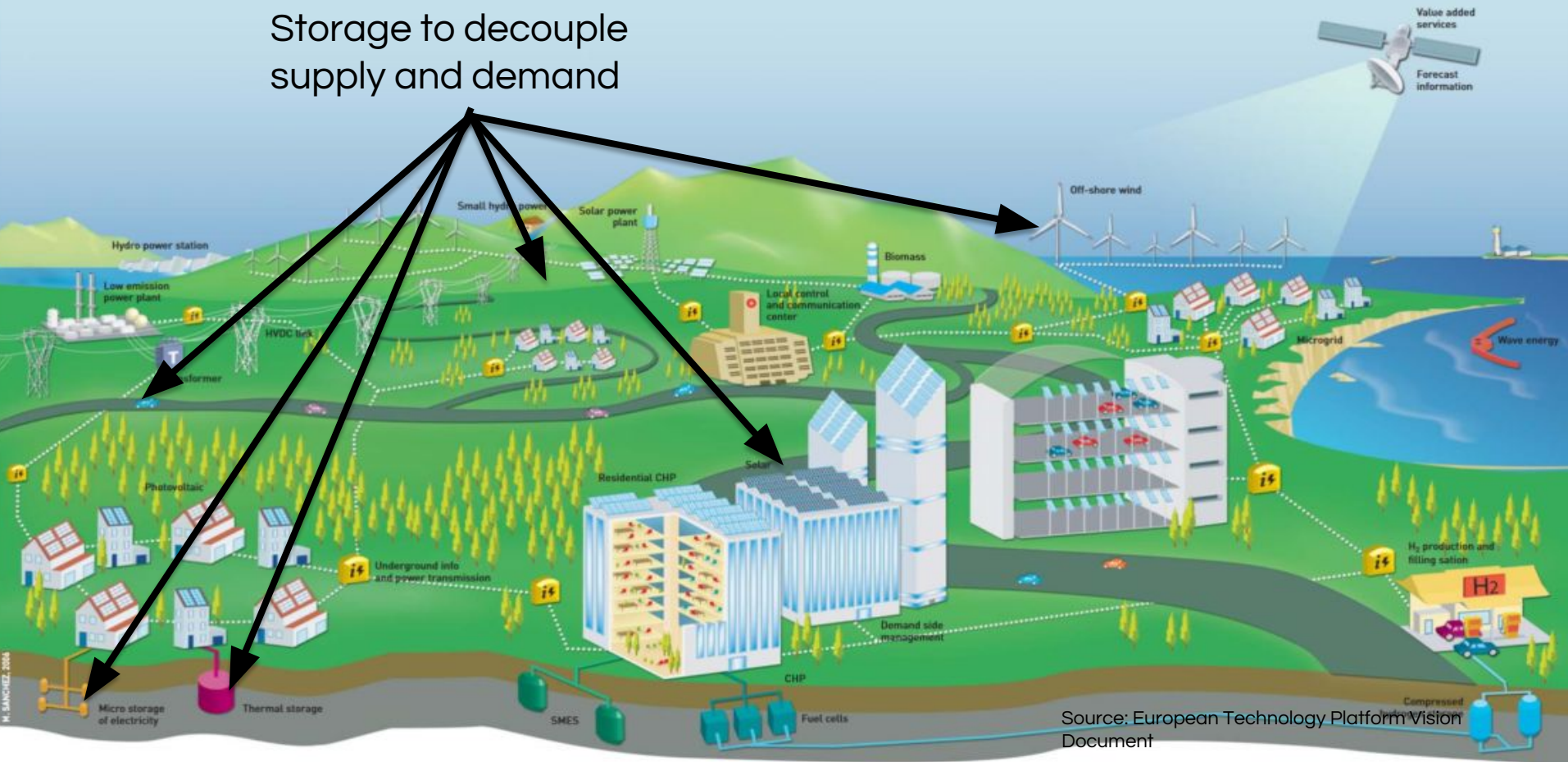
Source: European Technology Platform Vision Document

Pervasive sensing,  
communication, control



Source: European Technology Platform Vision Document

# Storage to decouple supply and demand



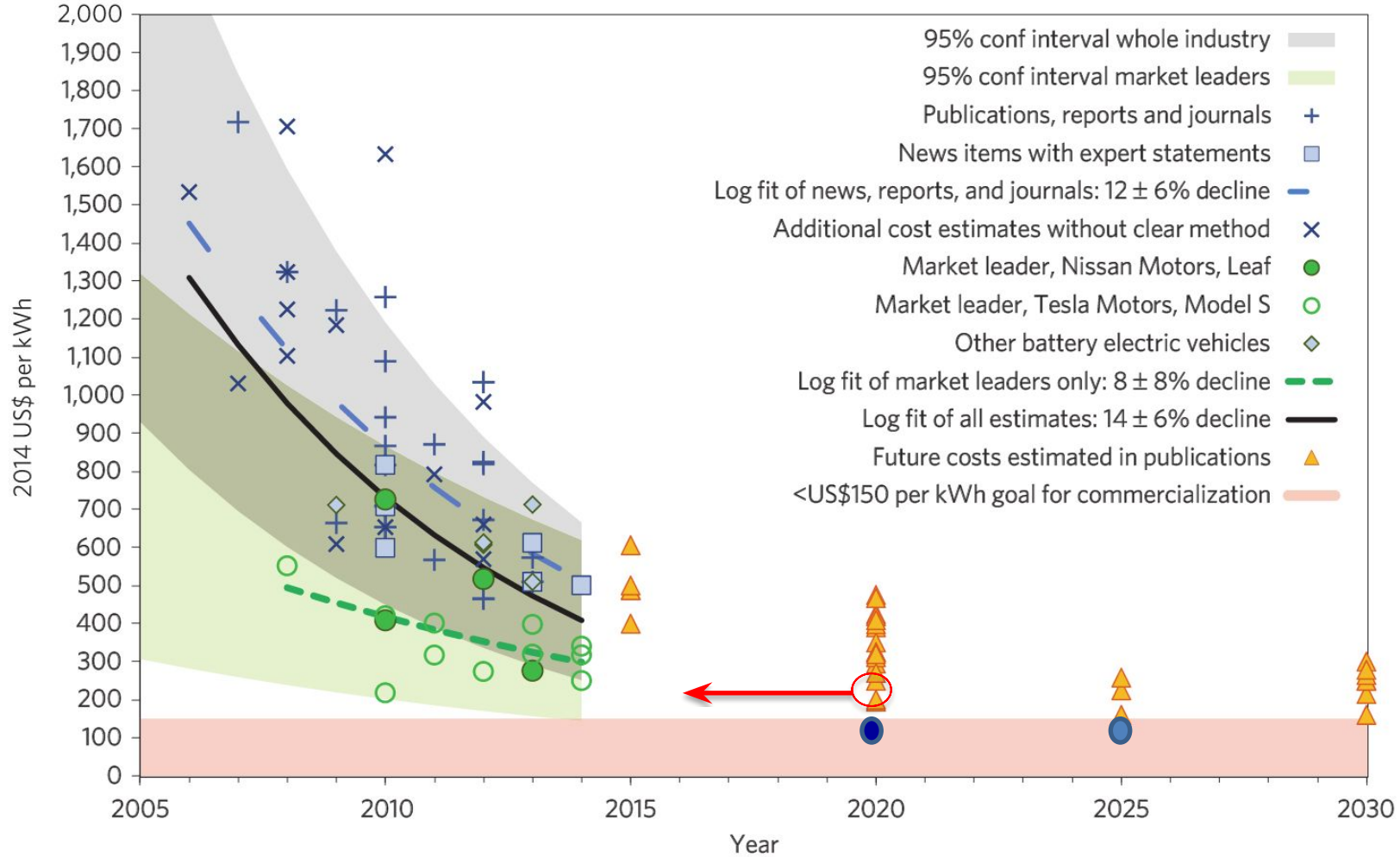
# Storage: A Hot Area

Global investment in energy storage technologies to reach **\$122 Billion** by 2021



Source: Pike Research

# Battery Costs: Current and Projections



Change: 2014

Tesla/Panasonic and GM/LG Chem battery costs were already (in 2016) down to the lowest projections for 2020!

# Why Storage?

Storage **decouples** supply and demand. Allows

**Reliability**

for large scale  
renewable integration

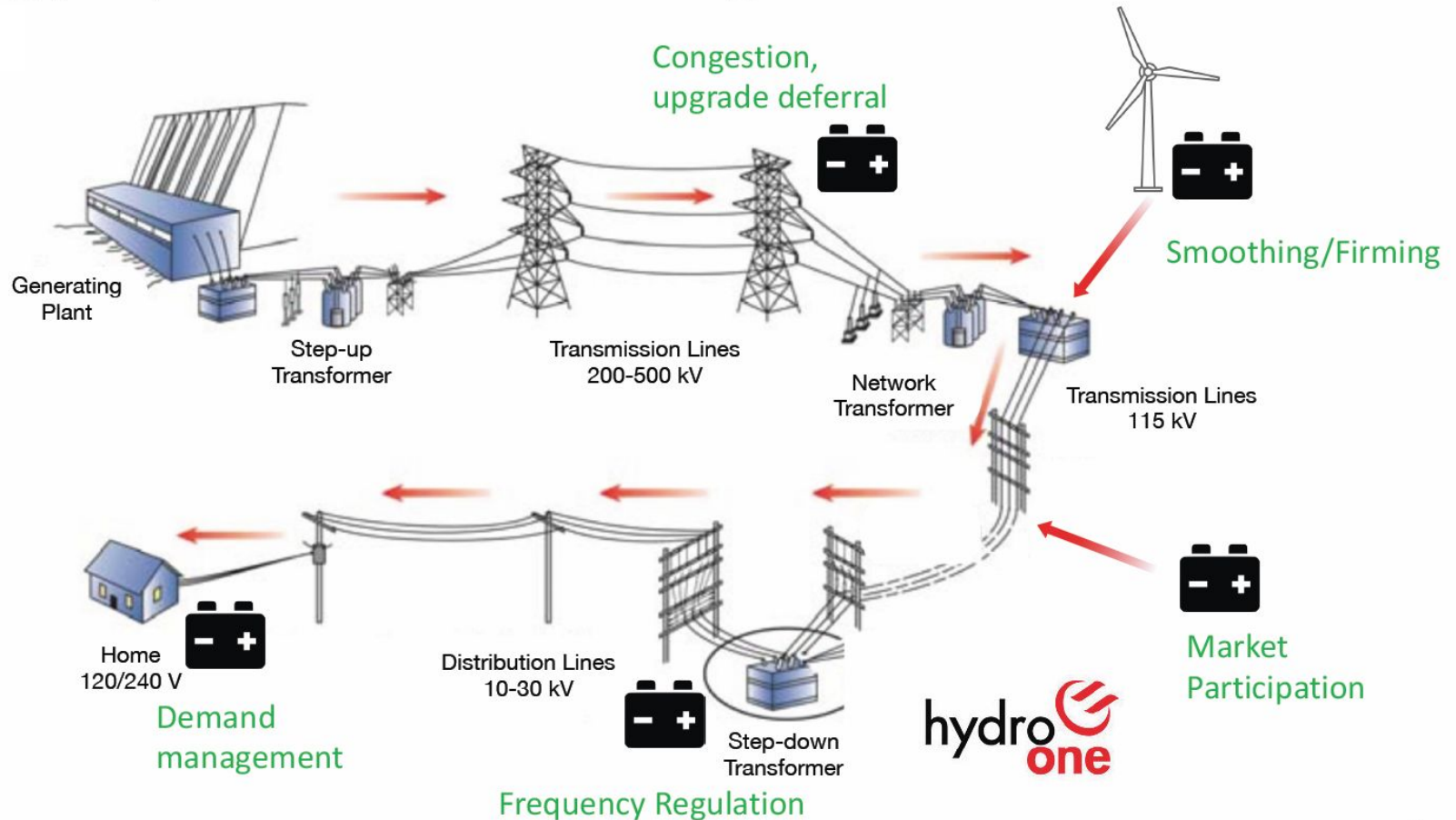
**Flexibility**

for energy management





# Applications



# Battery Models

## Electrochemical Models:

- Describes internal states of the battery by simulating chemical processes
- Useful for understanding and **designing** batteries

## Equivalent Circuit Models:

- Resistance-capacitance components to model voltage non-linearities
- Partial-differential equations
- Typically useful for **“small” simulations of energy systems**

## “Simplified Mathematical” Models:

- Black-box approach, model inputs and outputs
- Low-order polynomial functions
- Useful for **large-scale simulation, optimization of energy systems**

# Tractable Models For Optimization

## Accurate

- Required degree of accuracy depends on the application

## Tractable and low computational complexity

- Explicitly described by polynomials. Linear is easiest to work with.

## Calibrated using spec

- Battery specifications sheet is readily available, avoid experiment-based parameter derivation which is cumbersome and does not scale

## Uses power as input

- Power is conserved, avoid having to explicitly model voltage/current transformations

## Integrates BMS (battery management system) functionality

- Model the cells as well as the software that protects them from misuse.

# Our approach

Start with a model that meets 4/5 requirements

- Accurate, spec-calibrated, power-based, integrated BMS, but is not explicit and based on polynomials
- Power-based Integrated (PI) model (*F. Kazhamiaka, S. Keshav, C. Rosenberg, and K-H. Pettinger, “Simple Spec-Based Modelling of Lithium-Ion Batteries”, accepted to IEEE Transactions on Energy Conversion, April 2018.*)

Explore different ways to approximate the complex parts of the PI model

- Approximate using polynomials of degree 0 (constants) through 4 (quartics)
- Get a sense of what is lost with each approximation by comparing with the PI model

# Our Contributions

- Derive explicit models from the PI model
- Explore the effects of model accuracy with respect to the battery application
- Calibrate and validate the benchmark used by almost everyone

Note: All of this work is validated with an extensive measurement campaign

- Two Lithium-ion technologies
- Two cells per technology
- Charge/discharge test profiles exploring full capabilities of each cell
- Test profile resembling realistic usage

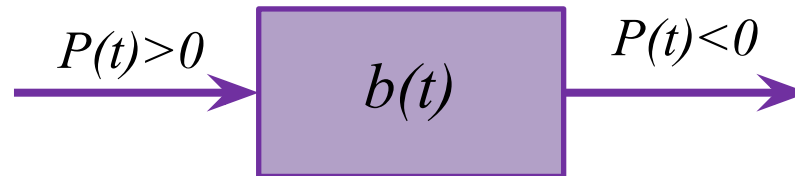
# Disclaimer

We do not model:

- State of health (degradation)
- Battery lifetime
- Temperature effects

# A Storage Model Based on First Principle

The storage has some **capacity**  $B$  in Wh. At time  $t$ , it is charged with power  $P(t) > 0$  or discharged with power  $P(t) < 0$ . Its content is  $b(t)$



The **ideal** behavior is:

$$0 \leq b(t+\delta) = b(t) + P(t) \delta \leq B$$

where  $\delta$  is the time-slot duration

However, it is important to consider **imperfections**, such as:

- charging/discharging speed limits
- energy conversion/inversion efficiency
- capacity limits

**The benchmark:** one input  $P(k)$ , one state variable  $b(k)$

$$b(k) = b(k - 1) + \Delta_E(k)$$

$$\Delta_E(k) = \begin{cases} \eta_c P(k) \delta & : P(k) \geq 0 \\ \eta_d P(k) \delta & : P(k) < 0 \end{cases}$$

$$u_d \leq P(k) \leq u_c$$

$$a_1 \leq b(k) \leq a_2$$

**Capacity limits**

Red and blue are for system parameters

**(In) efficiency:**  
losses in energy conversion

**(Dis)charging limits:**  
To avoid damaging storage, the **BMS** might prevent charging or discharging too quickly

**The PI model:** one input  $P(k)$ , one state variable  $b(k)$ , two internal variables  $I(k)$  and  $V(k)$

$$b(k) = b(k - 1) + \Delta_E(k)$$

$$\Delta_E(k) = \begin{cases} \eta_c(I(k), V(k)) P(k) \delta & : P(k) \geq 0 \\ \eta_d(I(k), V(k)) P(k) \delta & : P(k) < 0 \end{cases}$$

$$\eta_c(I(k), V(k)) = 1 - \frac{I(k) R_{ic}}{V(k)} : I(k) \geq 0$$

$$\eta_d(I(k), V(k)) = 1 - \frac{I(k) R_{id}}{V(k)} : I(k) < 0$$

$$V(k) = M(b(k), I(k))$$

$$I(k) = \frac{P(k)}{V(k)}$$

$$\alpha_d \leq I(k) \leq \alpha_c$$

$$a_1(I(k)) \leq b(k) \leq a_2(I(k))$$

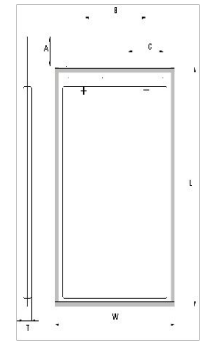
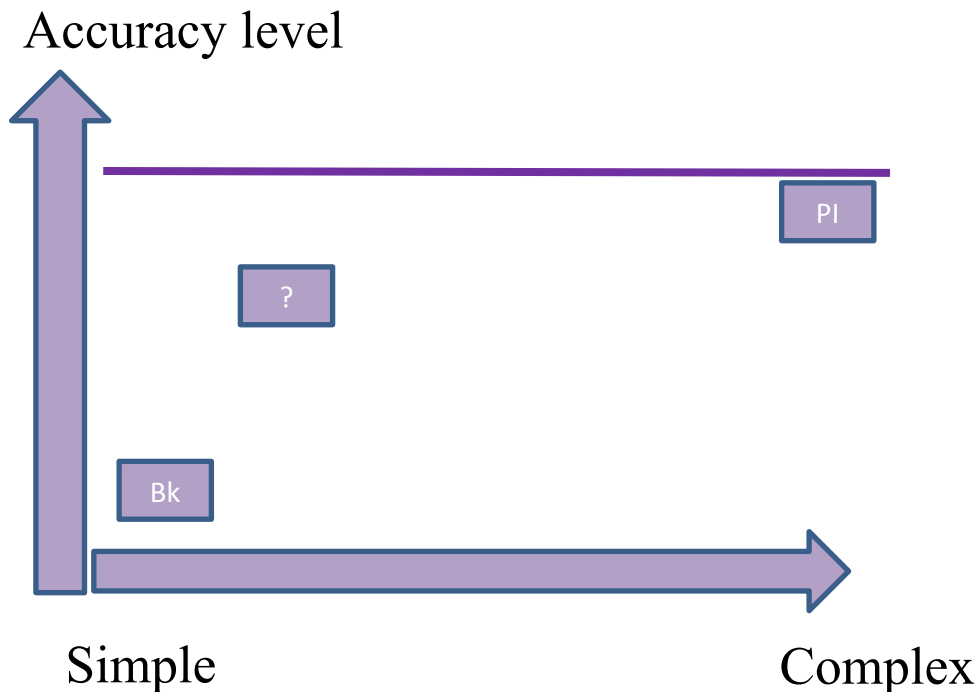
**Main differences:**

- voltage and current are internal variables,
- the inefficiencies and the capacity limits are no more constant
- the (dis)charging limits are on current
- Introduction of the empirical function  $z = M(x, y)$



# Two Main Issues

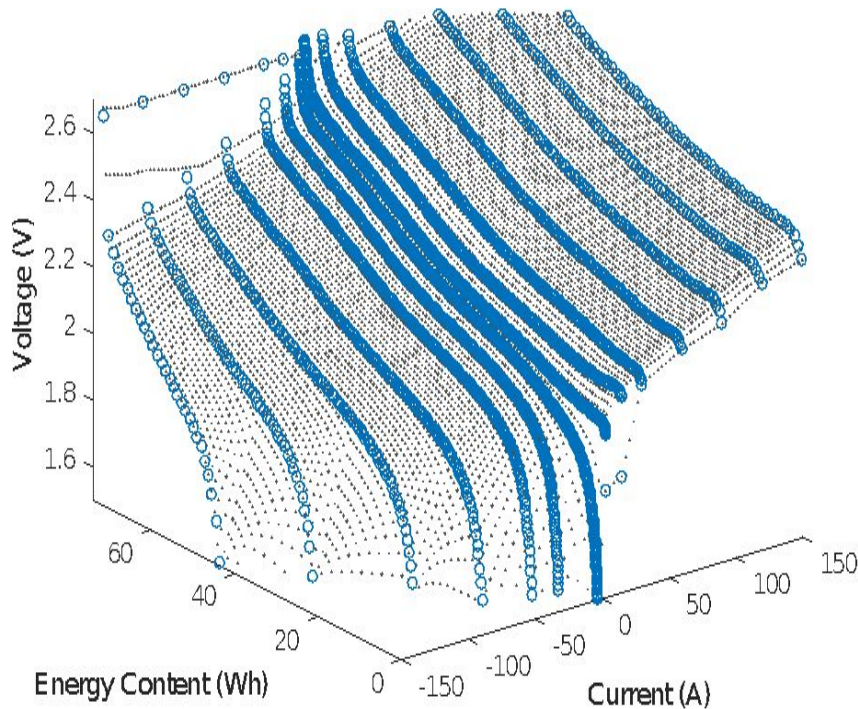
- Calibrating these models, i.e., selecting the parameters out of the spec sheet.
- Validating them: is the benchmark good enough?



## Technical Data

Nominal Capacity	30 Ah (measured at C/10 discharge rate, RT)
Nominal Voltage	2,3 V
Voltage range	1,7 V to 2,7 V
Impedance (1 kHz)	< 2 mOhm
Dimensions	Length (L) 287 mm ± 1 mm Width (W) 178,5 mm ± 1 mm (163 mm main body) Thickness (T) 12 mm +0,0/-0,5 mm
Weight	1100 g
Volume	475 ml
Housing	Foil packaging
Tabs	Aluminium (+ Pole), Ni-coated Copper (- Pole)
Length	33 mm ± 1 mm
Distance	90 mm ± 0,25 mm
Width	50 mm ± 0,5 mm
Thickness	0,2 mm ± 0,02 mm
Expected lifetime	Up to 15,000 cycles (at 1C charge/discharge full DoD and RT)
Expected calendar life	20 years (at RT)
<b>Charge</b>	
Charging method	CCCV (constant Voltage with limited current)
Max. charge voltage	2,7 V (+0,05 V)
Recommended charge current	30 A (1C)
Max. charge current	120 A (4C)
End of charge	U = 2,7 V and I < C/10
Max. temperature range	-20°C to +55°C
<b>Discharge</b>	
Recommended discharge current	30 A (1C)
Max. discharge current	120 A (4C)
End of discharge Voltage	1,7 V
Max. temperature range	-20°C to +55°C

# The Function $M(\cdot)$



$M$  surface represents viable combinations of cell voltage, energy content, and applied current

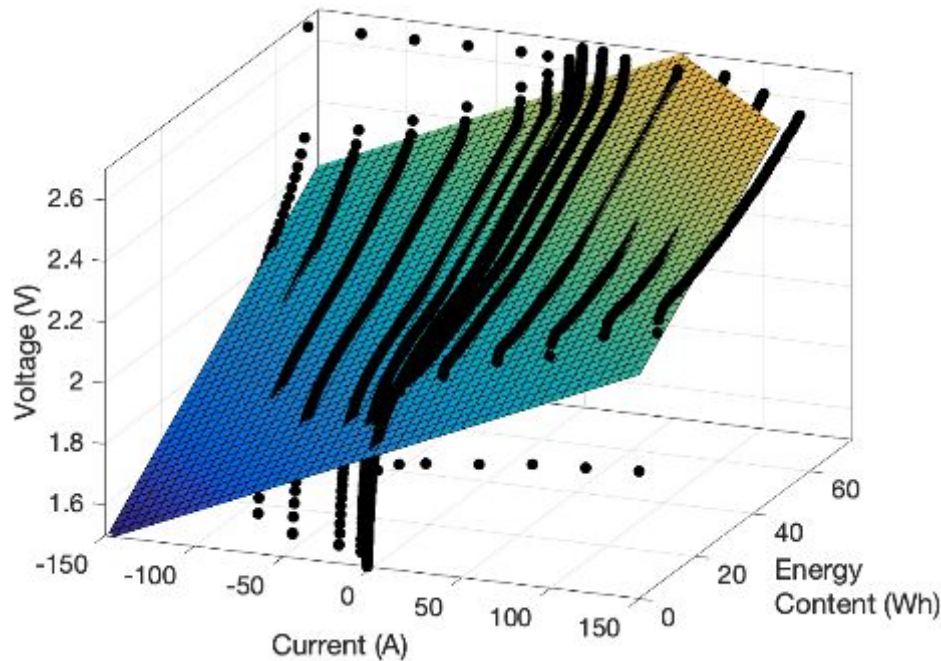
For  $P(k) > 0$ , we need to find the intersection between the surface defined by  $M(\cdot)$  and the surface defined by:

$$b(k) = b(k-1) + P(k) - I^2(k)R_{ic}$$

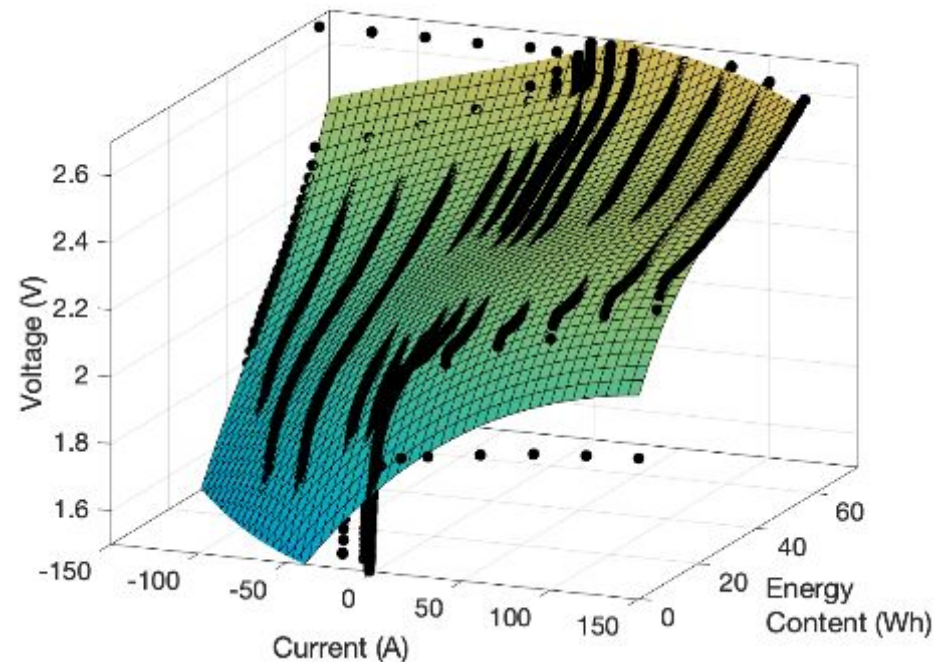
$$V(k) = M(b(k), I(k))$$

# 1. Voltage Function Approximation

In the PI model, the M function is an interpolation of points obtained from the spec. We can approximate it as a bivariate polynomial.



Linear approximation

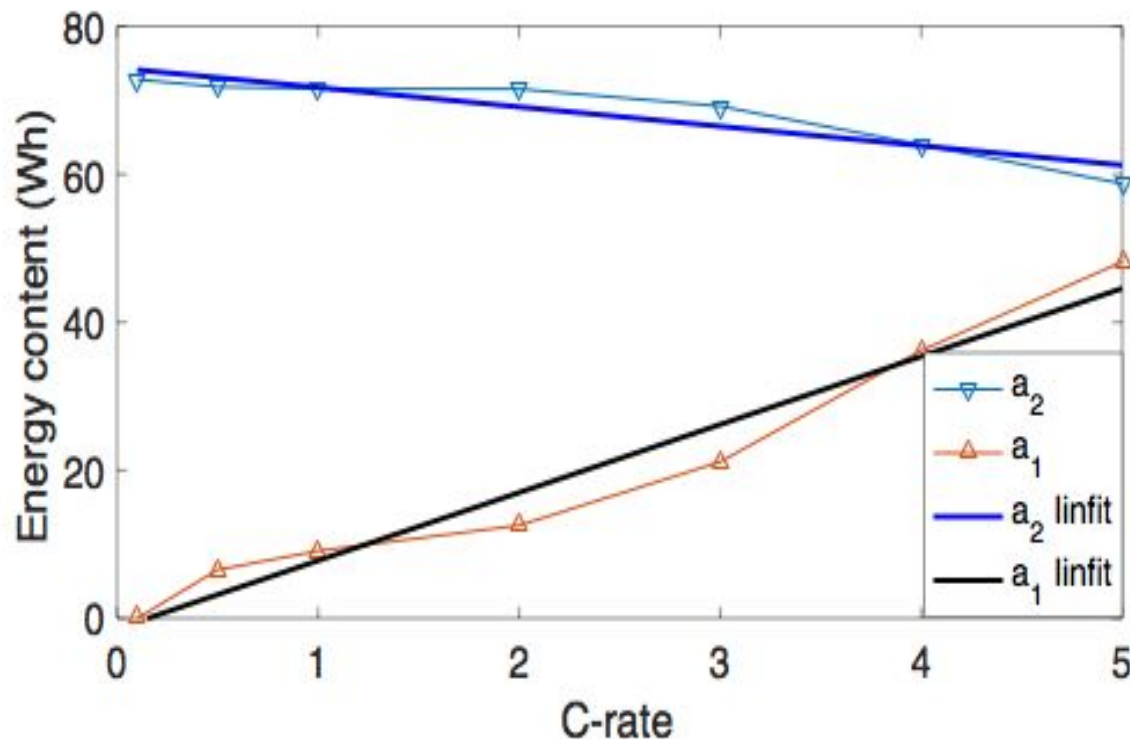


Cubic approximation

## 2. Energy Limit Functions

$$a_1(I(k)) \leq b(k) \leq a_2(I(k))$$

$a_1$  and  $a_2$  are functions of the current (approximately linear)



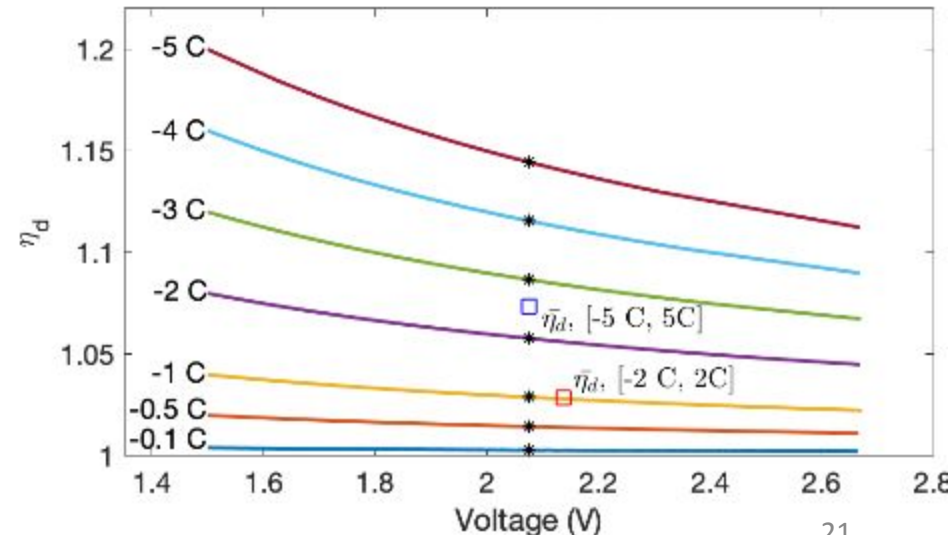
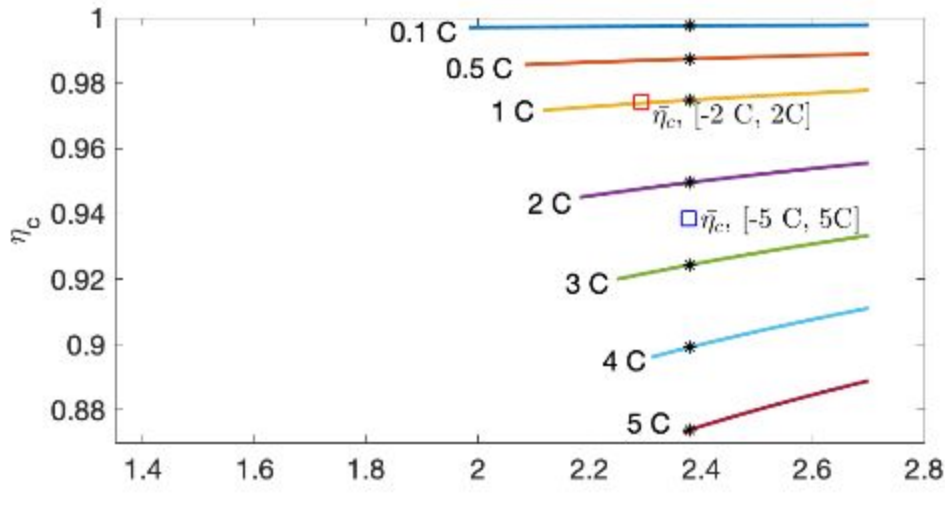
# 3. Efficiency Functions

$$\eta_c(I(k), V(k)) = 1 - \frac{I(k)R_{ic}}{V(k)} : I(k) \geq 0$$

$$\eta_d(I(k), V(k)) = 1 - \frac{I(k)R_{id}}{V(k)} : I(k) < 0$$

We approximate the efficiency functions using constants or lines.

Constant approximations look bad, but that's what people have been doing! And not as carefully as shown here!



# Four models

V/E/ $\eta$  notation: Voltage, energy limit, and efficiency approximation  
 C: constant, L: linear, Q: quadratic (in terms of model variables)

Model	Approximations		
	Voltage	Energy Content Limits	Efficiency
C/C/C	$V = \begin{cases} V_{nom,d} & : P < 0 \\ V_{nom,c} & : P \geq 0 \end{cases}$	$\begin{aligned} \bar{a}_1 \\ \bar{a}_2 \end{aligned}$	$\begin{aligned} \bar{\eta}_d \\ \bar{\eta}_c \end{aligned}$
C/L/C	$V = \begin{cases} V_{nom,d} & : P < 0 \\ V_{nom,c} & : P \geq 0 \end{cases}$	$\begin{aligned} a_1(P) &= u_1(P/V_{nom,d}) + v_1 \\ a_2(P) &= u_2(P/V_{nom,c}) + v_2 \end{aligned}$	$\begin{aligned} \bar{\eta}_d \\ \bar{\eta}_c \end{aligned}$
C/L/L	$V = \begin{cases} V_{nom,d} & : P < 0 \\ V_{nom,c} & : P \geq 0 \end{cases}$	$\begin{aligned} a_1(P) &= u_1(P/V_{nom,d}) + v_1 \\ a_2(P) &= u_2(P/V_{nom,c}) + v_2 \end{aligned}$	$\begin{aligned} \eta_d(P) &= 1 - PR_{id}/V_{nom,d}^2 \\ \eta_c(P) &= 1 - PR_{ic}/V_{nom,c}^2 \end{aligned}$
L/L/Q	$V = x_{00} + x_{10}I + x_{01}b$	$\begin{aligned} a_1(I) &= u_1I + v_1 \\ a_2(I) &= u_2I + v_2 \end{aligned}$	$\begin{aligned} \eta_d(I, V) &= 1 - IR_{id}/V \\ \eta_c(I, V) &= 1 - IR_{ic}/V \end{aligned}$

C/C/C is equivalent to the benchmark

# Four Models: Complexity

Consider an optimization problem where  $b$  and  $P$  are variables.

Complexity of each model w.r.t. the variables

- C/C/C: Linear (hence its popularity)
- C/L/C: Linear ★
- C/L/L: Quadratic (efficiency is a function of the power)
- L/L/Q: Cubic (efficiency is a function of power and voltage)

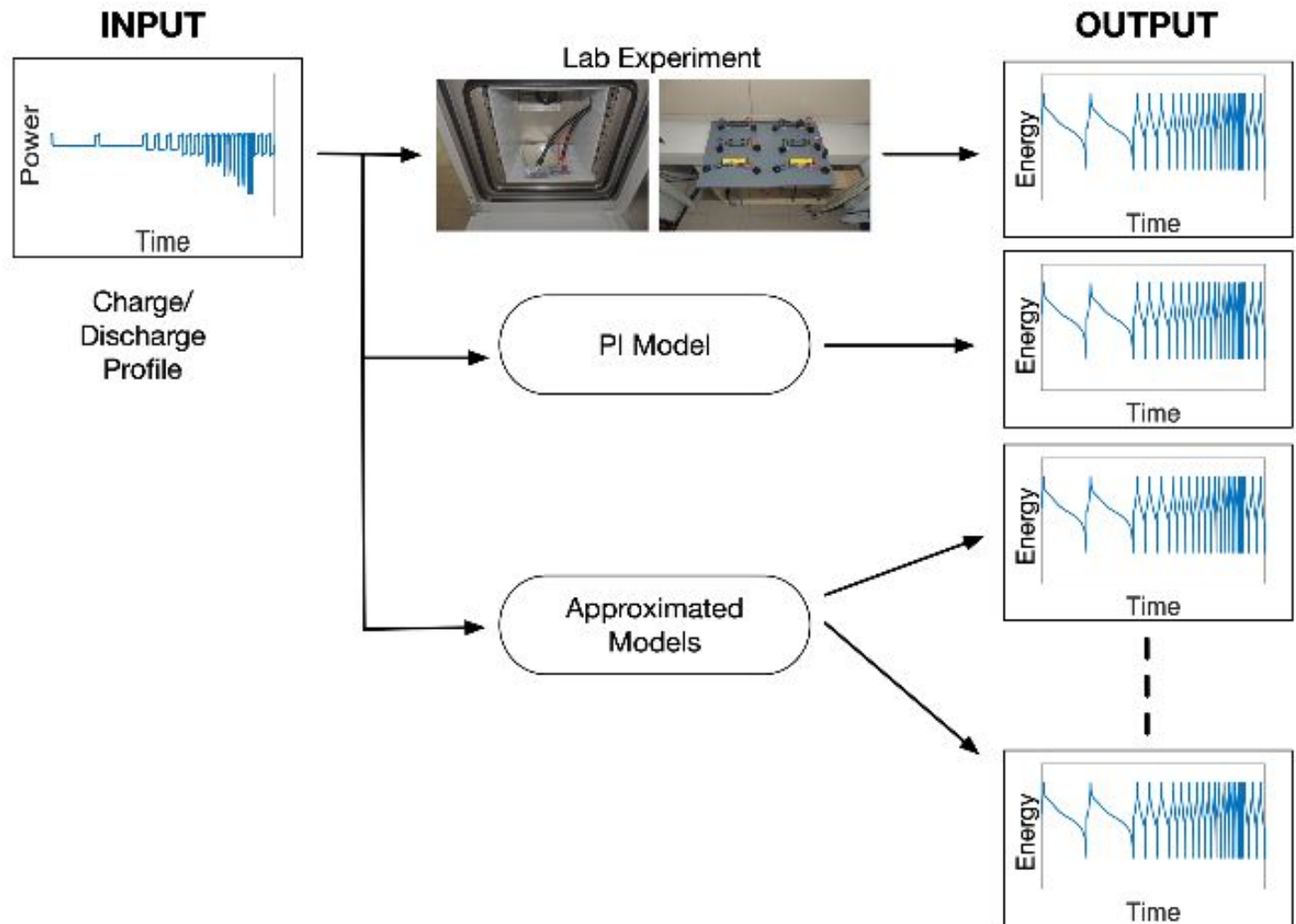
# Evaluation

## Metric: Energy

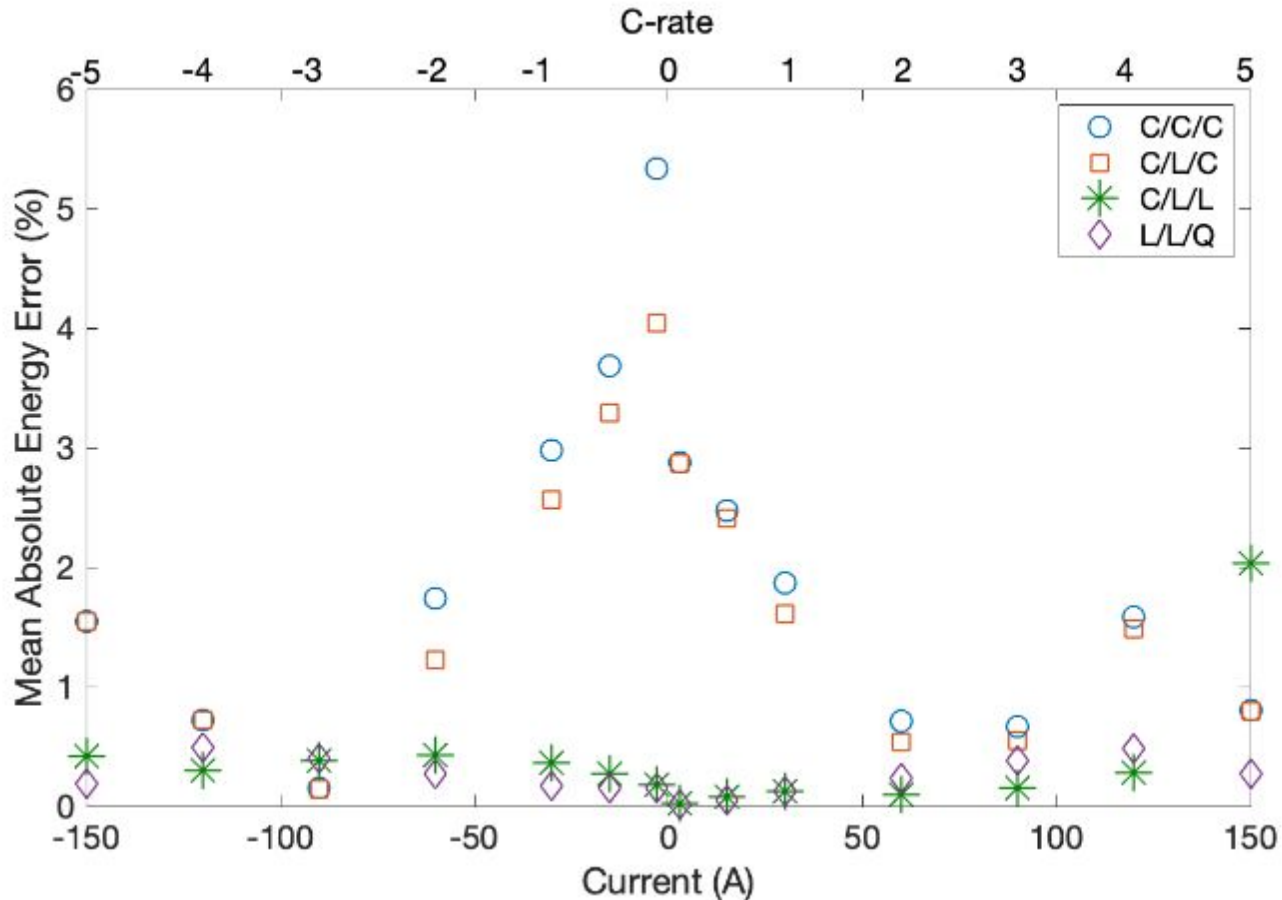
- Compute the mean absolute energy error (MAEE) when cycling the battery at constant current
- Ground truth: PI model.
- Battery chemistries: Lithium Titanate and Lithium Ferrous Phosphate.



# Evaluation



# Evaluation: Lithium-Titanate

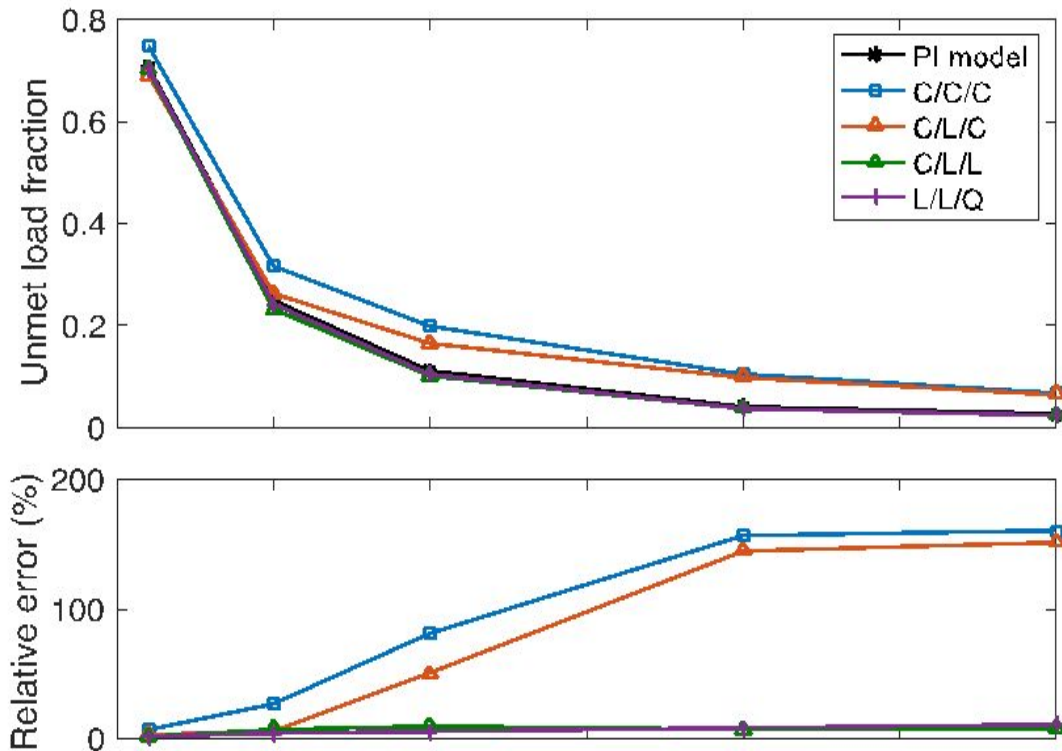


Models perform in order of the degree of their complexity.

# Evaluation on Applications

- How do we convince people to adopt our models?
- Accuracy metrics aren't always convincing...
- Lets see how model results differ for two applications
  - ❖ **Solar farm**: participating in electricity market in the form of constant hourly production
    - Key variable: The amount of energy that the farm committed to providing, but did not deliver (unmet load)
  - ❖ **Regulation**: ancillary service, focus on discharging
    - Key variable: Maximum power that we can guarantee to provide.

# Solar Farm

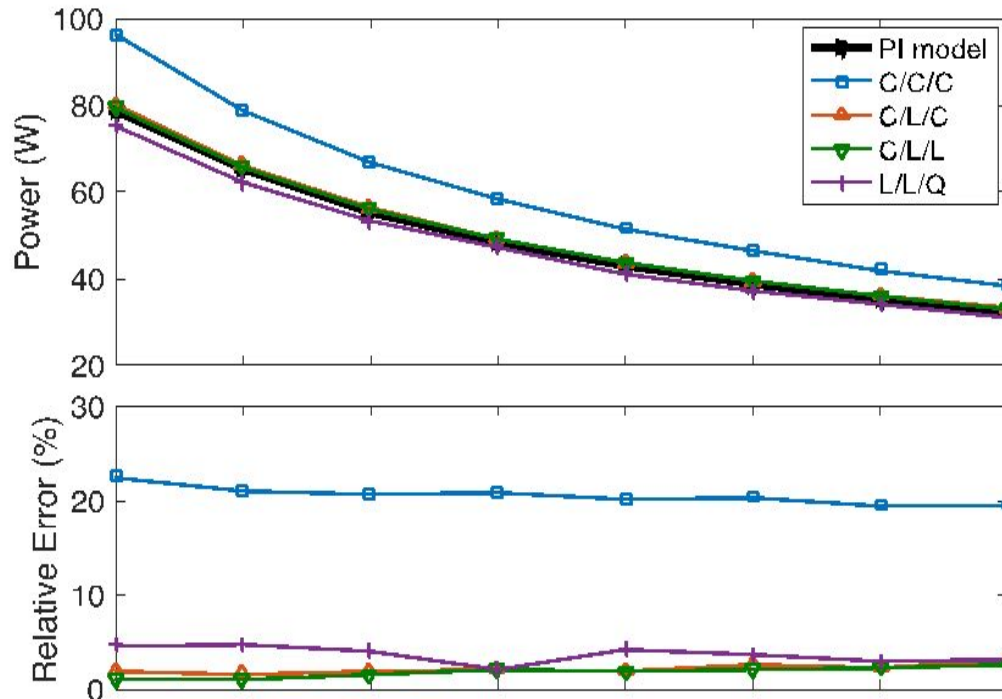


C/L/L and L/L/Q results are almost identical

Minimum # of cells to get 25% unmet load:

- PI: 50
- **C/C/C: 77**
- C/L/C: 56
- **C/L/L: 48**
- L/L/Q: 49

# Regulation



This is the maximum power that we could guarantee to provide for the length of the contract, if the battery starts at 50% capacity.

All models perform quite well, except for C/C/C, hence the winner is **C/L/C**

# What Did We Learn?

- Not trivial to calibrate even the benchmark
- C/L/C > C/C/C while remaining linear
- Understanding the approximations made in simpler models is crucial.

# What Is Next?

- Experiments are under-way to validate our models for different Lithium-ion chemistries, as well as other battery technologies
  - ❖ Lead-Acid,
  - ❖ Redox-Flow
  - ❖ Sodium-Nickel-Chloride
- How to take into account temperature? state of health?

# What next?